

$$mg = \rho_{\text{object}} V_{\text{object}} g, \quad B = \rho_{\text{fluid}} V_{\text{fluid}} g$$

Floating, $V_{\text{object}} \neq V_{\text{fluid}}$

Floating \Rightarrow equilibrium

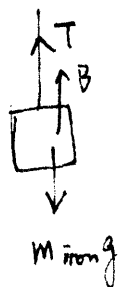


$$B - mg = 0, \quad B = mg$$

$$\rho_{\text{fluid}} V_{\text{fluid}} g = \rho_{\text{object}} V_{\text{object}} g$$

$$\frac{\rho_{\text{object}}}{\rho_{\text{fluid}}} = \frac{V_{\text{fluid}}}{V_{\text{object}}}$$

#43



Top scale reads T

$$T + B - M_{\text{iron}} g = 0$$

$$T = M_{\text{iron}} g - B$$

$$= m_{\text{iron}} g - \rho_{\text{fluid}} V_{\text{fluid}} g$$

Block is completely submerged

$$V_{\text{fluid}} = V_{\text{iron}} = \frac{M_{\text{iron}}}{\rho_{\text{iron}}}$$

$$T = m_{\text{iron}} g - \rho_{\text{fluid}} \frac{M_{\text{iron}}}{\rho_{\text{iron}}} g$$

$$= m_{\text{iron}} g \left(1 - \frac{\rho_{\text{fluid}}}{\rho_{\text{iron}}} \right)$$

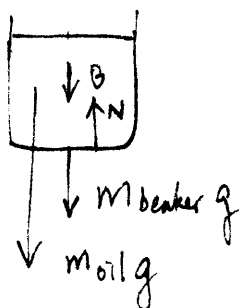
$$= 2(9.8) \left(1 - \frac{916}{7860} \right)$$

$$= 17.3 \text{ N}$$

Treat oil & beaker as one system

Newton's 3rd law, iron exerts B on liquid

Bottom scale reads N



$$N - m_{\text{oil}} g - m_{\text{beaker}} g - B = 0$$

$$N = m_{\text{oil}} g + m_{\text{beaker}} g + \rho_{\text{fluid}} \frac{M_{\text{iron}}}{\rho_{\text{iron}}} g$$

$$= (m_{\text{oil}} + m_{\text{beaker}} + \rho_{\text{fluid}} \frac{M_{\text{iron}}}{\rho_{\text{iron}}}) g$$

$$= \left(2 + 1 + 916 \frac{2}{7860} \right) 9.8$$

$$= 31.7 \text{ N}$$

Bernoulli's equation

$$\text{Work} = \Delta KE + \Delta PE$$

$$F_1 \Delta x_1 - F_2 \Delta x_2 = (P_1 A_1) \Delta x_1 - (P_2 A_2) \Delta x_2 = \frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2 + m g y_2 - m g y_1$$

$$A_1 \Delta x_1 = A_2 \Delta x_2 = V \text{ volume}$$

$$m = \rho V$$

$$P_1 V - P_2 V = \frac{1}{2} \rho V v_2^2 - \frac{1}{2} \rho V v_1^2 + \rho V g y_2 - \rho V g y_1$$

$$P_1 + \frac{1}{2} \rho v_1^2 + \rho g y_1 = P_2 + \frac{1}{2} \rho v_2^2 + \rho g y_2$$

$$P + \frac{1}{2} \rho v^2 + \rho g y = \text{constant}$$

#55.

$$\text{Flow rate} = 1.8 \times 10^{-4} = A_1 v_1$$

$$v_1 = \frac{1.8 \times 10^{-4}}{A_1} = \frac{1.8 \times 10^{-4}}{\pi \left(\frac{0.025}{2}\right)^2} = 0.37 \text{ m/s}$$

$$P_1 + \frac{1}{2} \rho v_1^2 + \rho g y_1 = P_2 + \frac{1}{2} \rho v_2^2 + \rho g y_2$$

$$\text{Horizontal flow } y_1 = y_2, \quad P_1 = P_{\text{atm}} + \rho g h_1$$

$$P_2 = P_{\text{atm}} + \rho g h_2$$

$$(P_{\text{atm}} + \rho g h_1) + \frac{1}{2} \rho v_1^2 = (P_{\text{atm}} + \rho g h_2) + \frac{1}{2} \rho v_2^2$$

$$v_2^2 = 2g(h_1 - h_2) + v_1^2 = 2(9.8)(0.1 - 0.05) + (0.37)^2$$

$$v_2 = 1.06 \text{ m/s}$$

$$\text{Flow rate} = 1.8 \times 10^{-4} = A_2 v_2$$

$$A_2 = \frac{1.8 \times 10^{-4}}{v_2}$$

$$\pi \left(\frac{d_2}{2}\right)^2 = \frac{1.8 \times 10^{-4}}{1.06} \Rightarrow d_2 = 0.0147 \text{ m}$$